

Micro flow reactor with prescribed temperature profile

Toward fuel Indexing and kinetics study based on multiple weak flames

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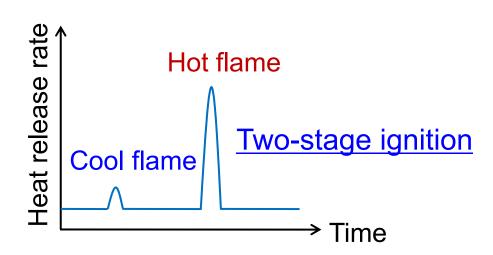
S. Minaev, N.I. Kim, T. Yokomori, H. Nakamura, S. Hasegawa, T. Tezuka T. Kataoka, Y. Tsuboi, H. Oshibe, A. Yamamoto, R. Tanimoto, M. Hori, K. Saruwatari, S. Suzuki, T. Kamada, X. Li, Y. Kizaki, T. Onishi and H. Takahashi



Background and objectives

For understandings ignition and combustion characteristics of practical fuels...

Data from
Shock tube and RCM
have been extensively used
Ignition delay

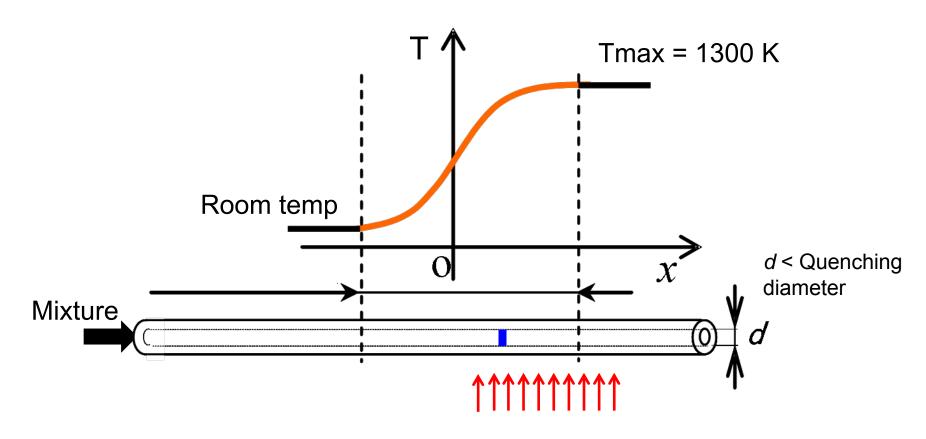


Micro flow reactor with prescribed temperature profile

Single or multiple weak flames



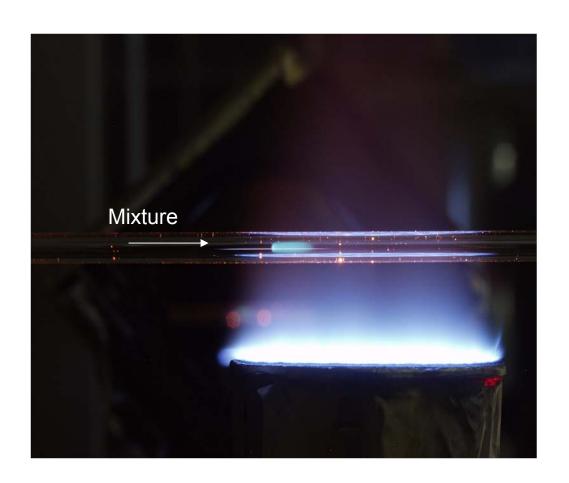
Micro flow reactor with prescribed temperature profile

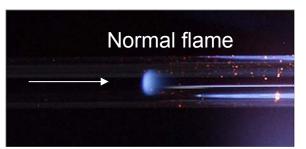


Stationary wall-temperature profile by an external heat source Inner diameter of the tube < conventional quenching diameter Gas phase temperature governed by wall temperature profile Laminar flow and constant pressure

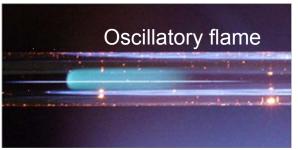


Flame behaviors in a micro flow reactor with a prescribed temperature profile

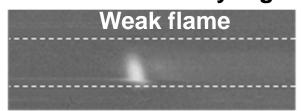




High velocity region



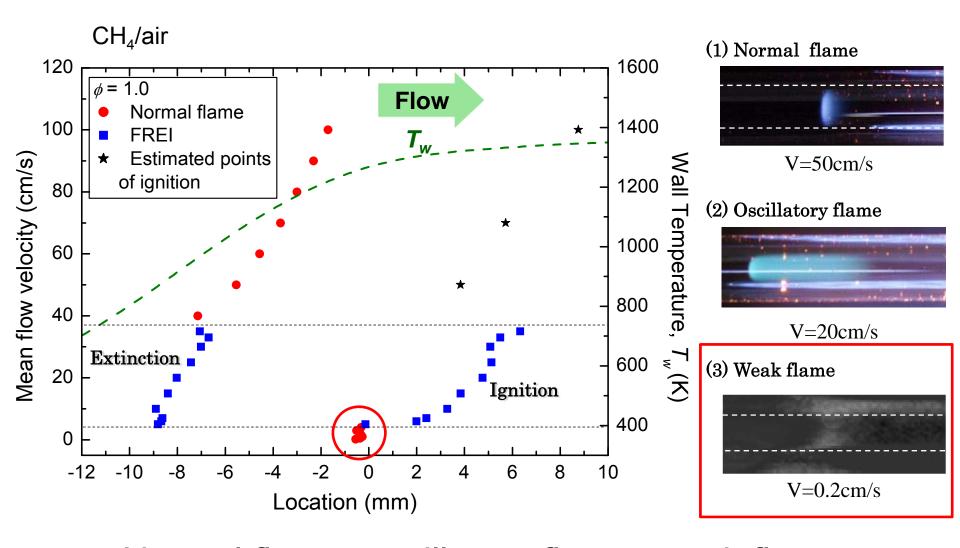
Intermediate velocity region



Low velocity region



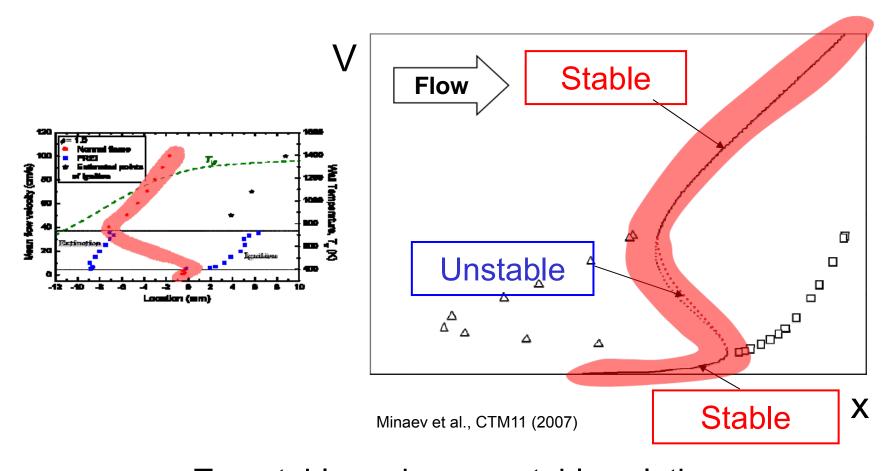
Three kinds of flame responses





Normal flame, oscillatory flame, weak flame

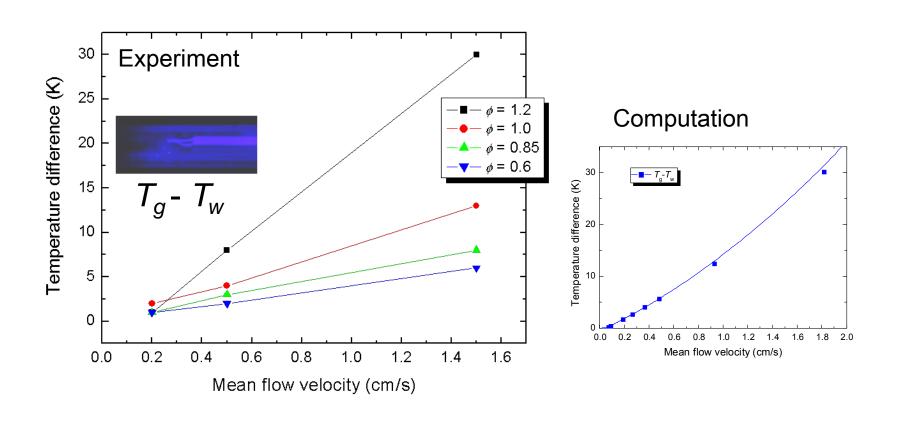
Theoretical S-shaped response





Two stable and one unstable solutions predicted theoretically → Weak flame corresponds to ignition branch

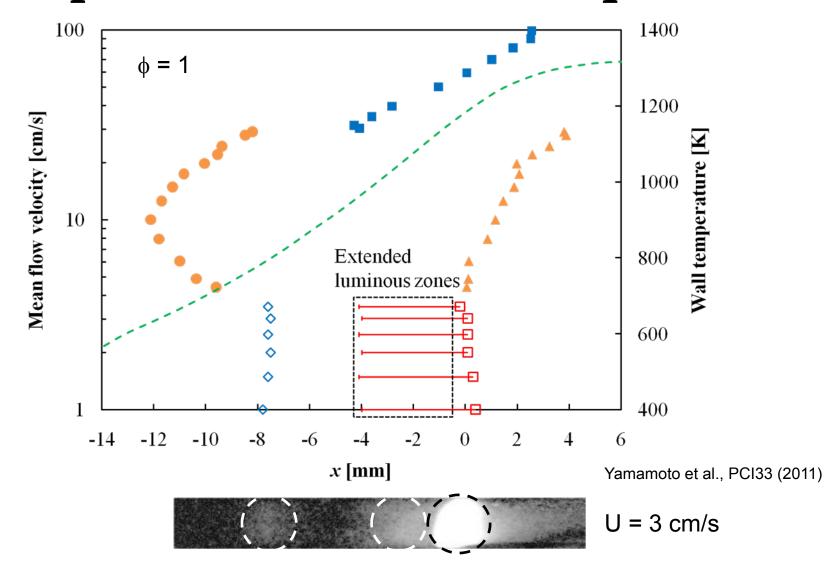
Lower limit of weak flames identified



At V = 0.2 cm/s, T_w = 1225 K, T_g - T_w < 2 K for CH_4 /air mixture Extremely small temperature increase near lower limit Flame position close to the ignition limit Weak flame location \rightarrow Ignition temperature



Triple weak flames, n-heptane





Triple stationary weak flames observed Weak flame location (temp.) insensitive to flow velocity

Computations (one-dimensional plug flow)

Code PREMIX with small modification

Gas-phase energy equation

$$\dot{M}\frac{dT}{dx} - \frac{1}{c_p}\frac{d}{dx}\left(\lambda A\frac{dT}{dx}\right) + \frac{A}{c_p}\sum_{k=1}^K \rho Y_k V_k c_{pk}\frac{dT}{dx} + \frac{A}{c_p}\sum_{k=1}^K \dot{\omega}_k h_k W_k - \frac{A}{c_p}\frac{4\lambda Nu}{d^2}(T_w - T_w) = 0$$

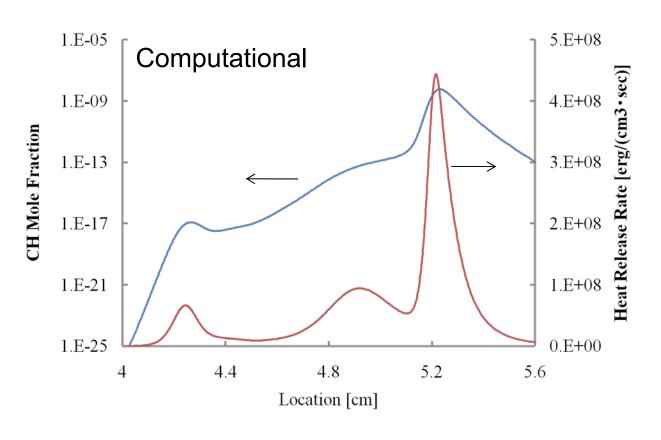
Heat transfer with the wall

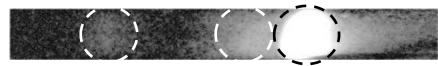
Reaction scheme *n*-heptane, reduced mechanism from LLNL (159 species, 1540 steps) Seiser et al., PCI 28 (2000)

<u>Conditions</u> Stoichiometric gaseous *n*-heptane/air mixture Experimental wall temperature profile was provided as Tw(x)

Flame position Peaks of heat-release-rate (HRR) [W/cm³] profile

Triple weak flames, n-heptane



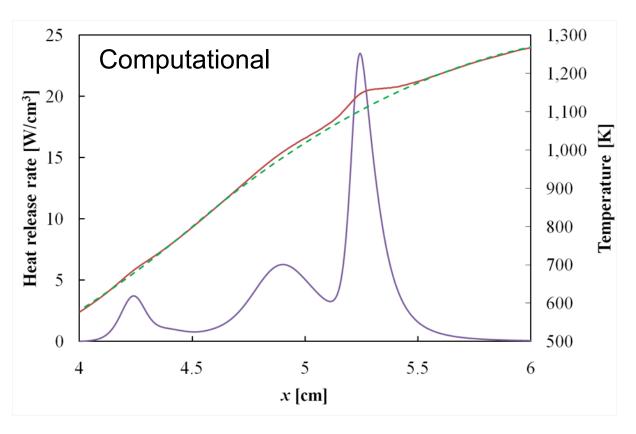


U = 3 cm/s



Three-stage heat release

Triple weak flames, n-heptane



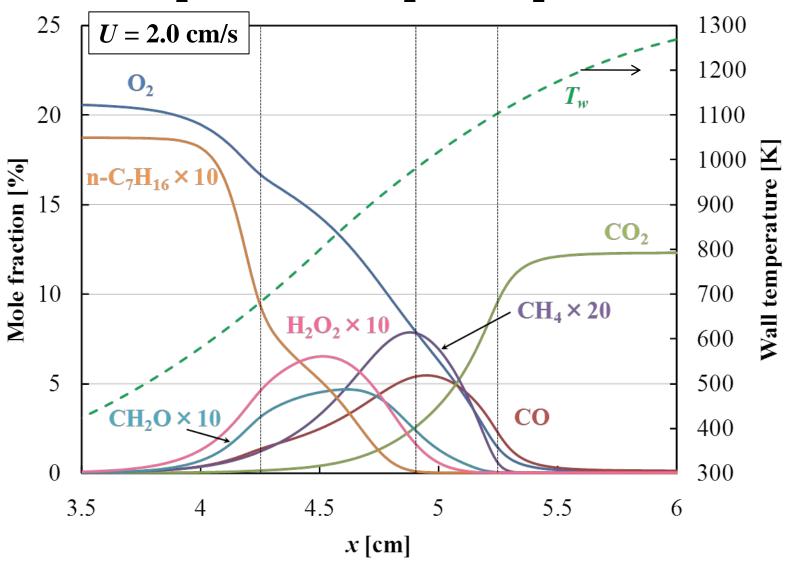


U = 3 cm/s



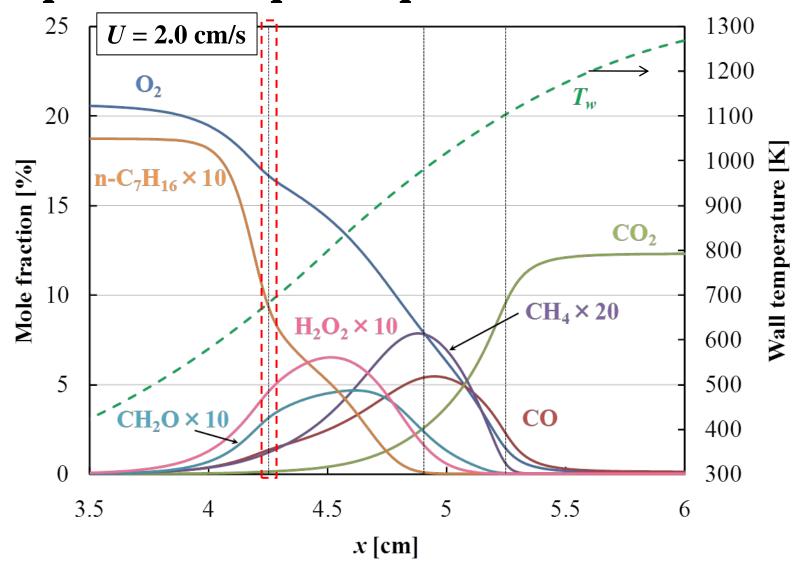
Three-stage heat release

Computational species profiles





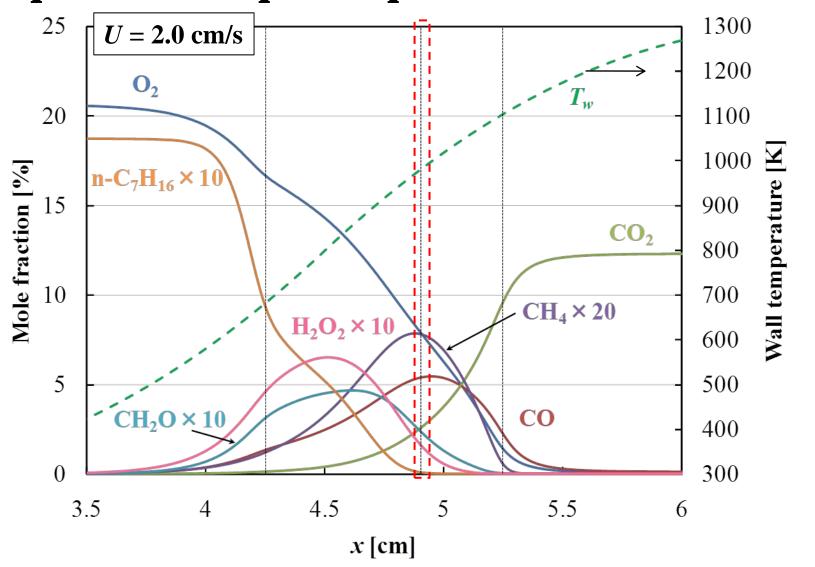
Computational species profiles -1st weak flame-





LTO: CH₂O, H₂O₂, CO, CH₄ produced

Computational species profiles -2nd weak flame-





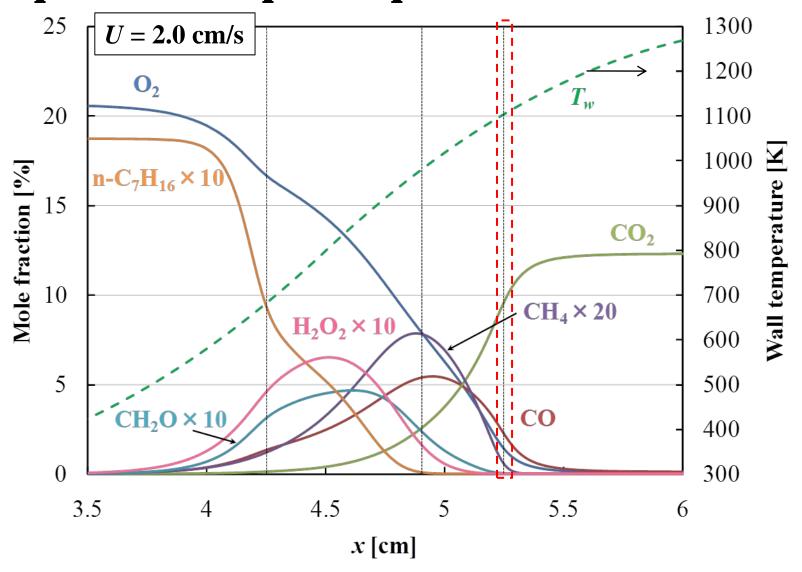
$$\mathbf{H}_2\mathbf{O}_2$$
 (+M) \Rightarrow 2OH (+M)

$$\mathbf{CH_2O} + \mathbf{OH} \Rightarrow \underline{\mathbf{HCO}} + \mathbf{H_2O}$$

$$\underline{\mathbf{HCO}} + \mathbf{O_2} \Rightarrow \mathbf{CO} + \mathbf{HO_2}$$



Computational species profiles -3rd weak flame-

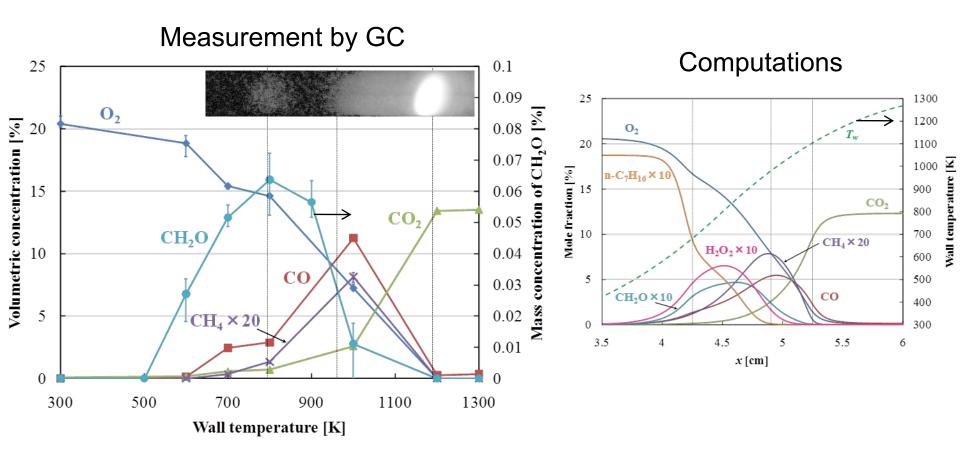




Full oxidations: $CO + OH \Rightarrow CO_2 + H$

Comparison: measurements and computations

(U = 2.0 cm/s)

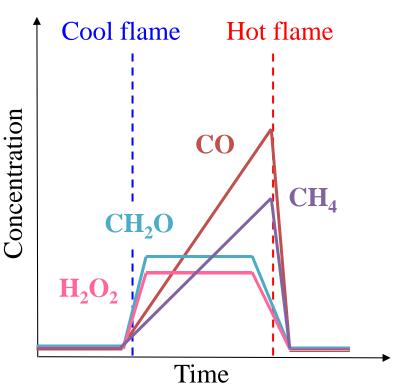


Three-stage oxidation process was experimentally confirmed by gas sampling

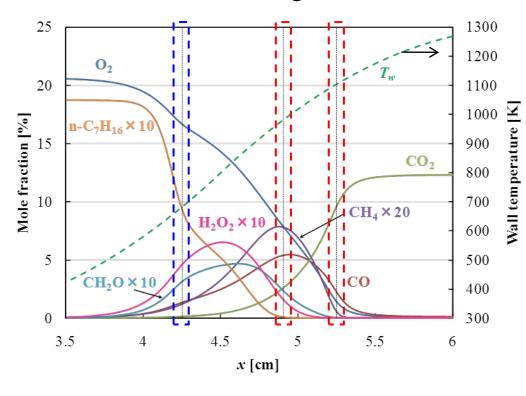


Interpretation of triple weak flames in MFR

Typical two-stage oxidation



Present three-stage oxidation



Typical two-stage oxidation: Cool flame + Hot flame

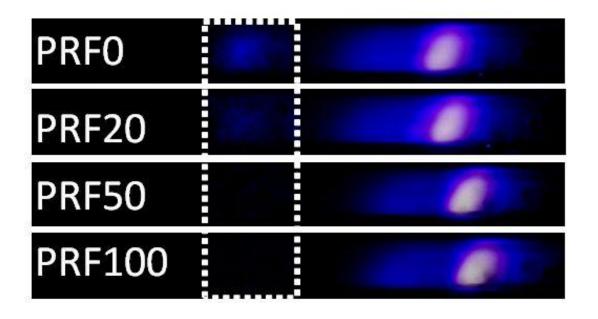
Three-stage oxidation: Cool flame + Separated hot flames

(Blue flame & Hot flame)



MFR applied for gasoline PRF

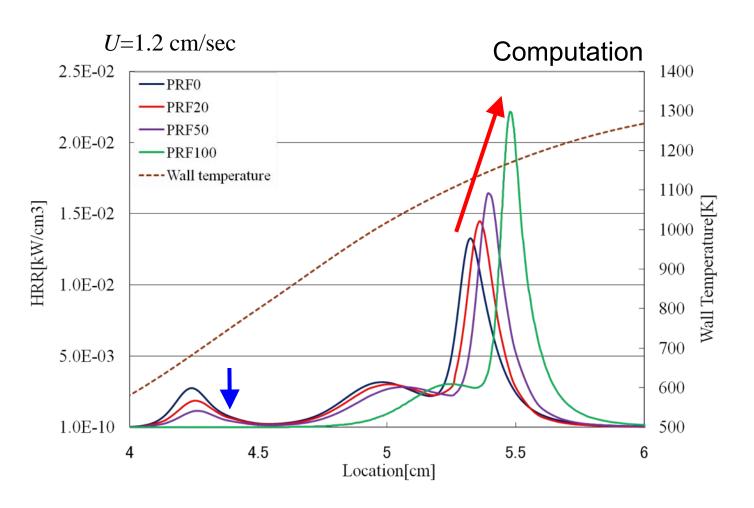
n-heptane + *iso*-octane (PRF)

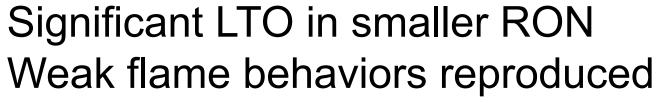


Appearances of multiple weak flame represent Research Octane Number



Weak flames at different RON

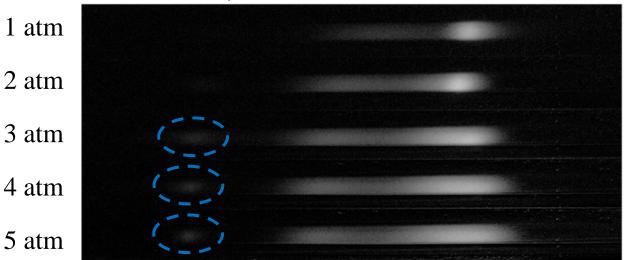


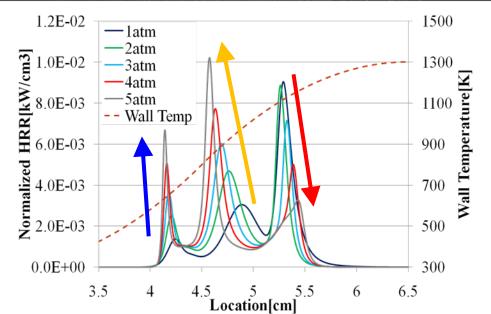




Weak flames at elevated pressures

PRF0 / air, *U*=2.0 cm/sec





PRF20, 50, 100 similar Tendencies but weaker LTO



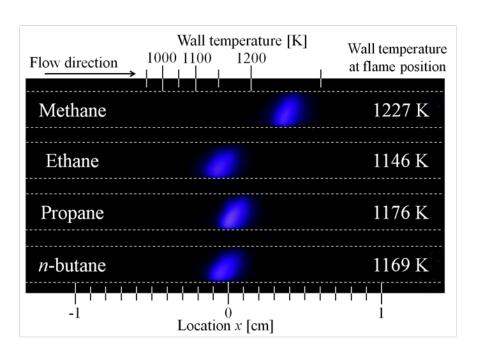
Fuels addressed

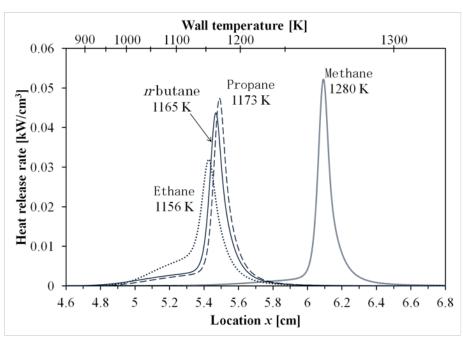
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methane (CH<sub>4</sub>)
DME (CH<sub>3</sub>OCH<sub>3</sub>)
n-heptane (C_7H_{16})
iso-octane (C_8H_{16})
toluene (C<sub>7</sub>H<sub>8</sub> or C<sub>6</sub>H<sub>5</sub>CH<sub>3</sub>)
methane (CH<sub>4</sub>)
ethane (C_2H_6)
propane (C<sub>3</sub>H<sub>8</sub>)
n-butane, iso-butane (C_4H_{10}) \rightarrow (Kamada et al., WIPP)
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Natural gas components

(Kamada et al., WIPP)



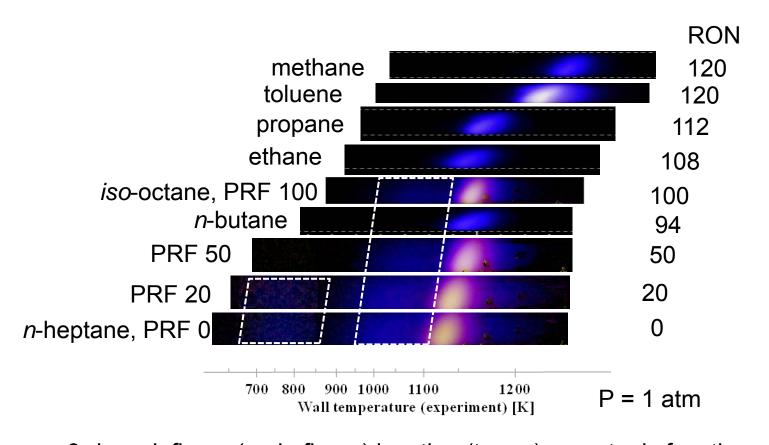


Similar single weak flame (hot flame) observed for each fuel Different flame locations Computations reproduced experimental observation



Weak flames at various RON

Data collected at slightly different conditions, i.e., flow velocity, exposure time, temperature profile





3rd weak flame (main flame) location (temp.) monotonic function of RON 2nd weak flame (blue flame) observable when RON < 100 1st weak flame (cool flame) observable when RON < 20

Conclusions and future, 1 of 2

Micro flow reactor with prescribed temperature profile was introduced

- -Three kinds of flame response (S-shaped)
- -Weak flame corresponds to ignition branch
- -Multiple weak flame utilized for fuel characterization
- -Multiple weak flames at elevated pressures
- -Appearances of weak flame correlated with RON

Conclusions and future, 2 of 2

Diesel fuels and Cetane numbers

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n-cetane (hexadecane, C_{16}H_{34})

iso-cetane (2,2,4,4,6,8,8-heptamethylnonane, C_{16}H_{34})

n-decane (C_{10}H_{22})

α-methylnaphthalene (C_{11}H_{10}) → (Suzuki et al., 5E06)
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Ethanol → (Nakamura et al., 1E02)

Syngas

Oxyfuel combustion → (Li et al., WIPP)

Effect of surface reaction → (Kizaki et al, WIPP)

PAH and soot

Optical diagnosis

LIF, CRDS for precise species profile measurements
Higher pressures



High pressure chamber (up to 20 bar) fabricated

Acknowledgements

IHI, IIC, HONDA R&D, JAXA, NEDO, HITACHI, TG, MEXT



Micro flow reactor now commercially available